

総 説

菊 地 光 雄

渡 辺 修

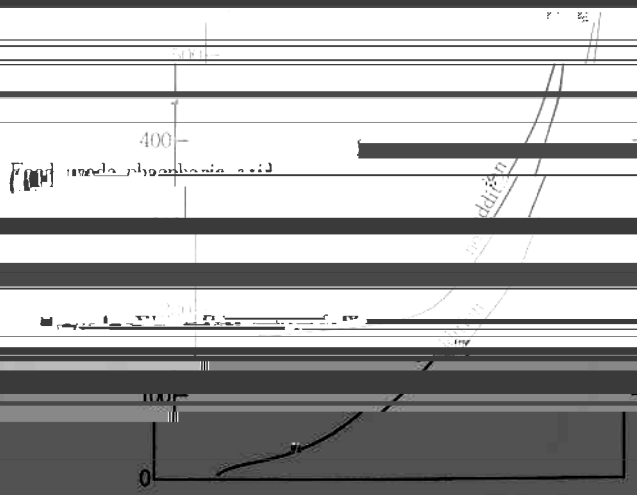
(1) 関連文籍

Recent Tondanor of Dainippon Kaisha, Ltd. (1941)

Dainippon Kaisha, Ltd. (1941)

Table 1 Comparison of P-3 and P-4 process

Stage Number	P-4 > P-3
Chemicals	Crude acid from wet-process plant
Extraction yield of P ₂ O ₅	(Feed)
	Extraction Battery
	Purification Battery
	Washing Battery
	Solvent Recovery
	Waste water treatment
	(Technical grade phosphoric acid)



Specific Gravity	1.39	1.58
P ₂ O ₅ (%)	33.5	
IT 710		

5980

0

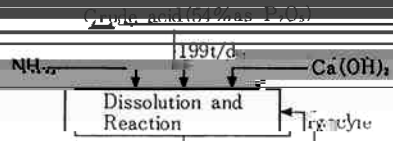
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Al

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NaOH battery

- - - Solvent Flow
 — Acid Flow

和 11、融解材の抽出装置（特許）

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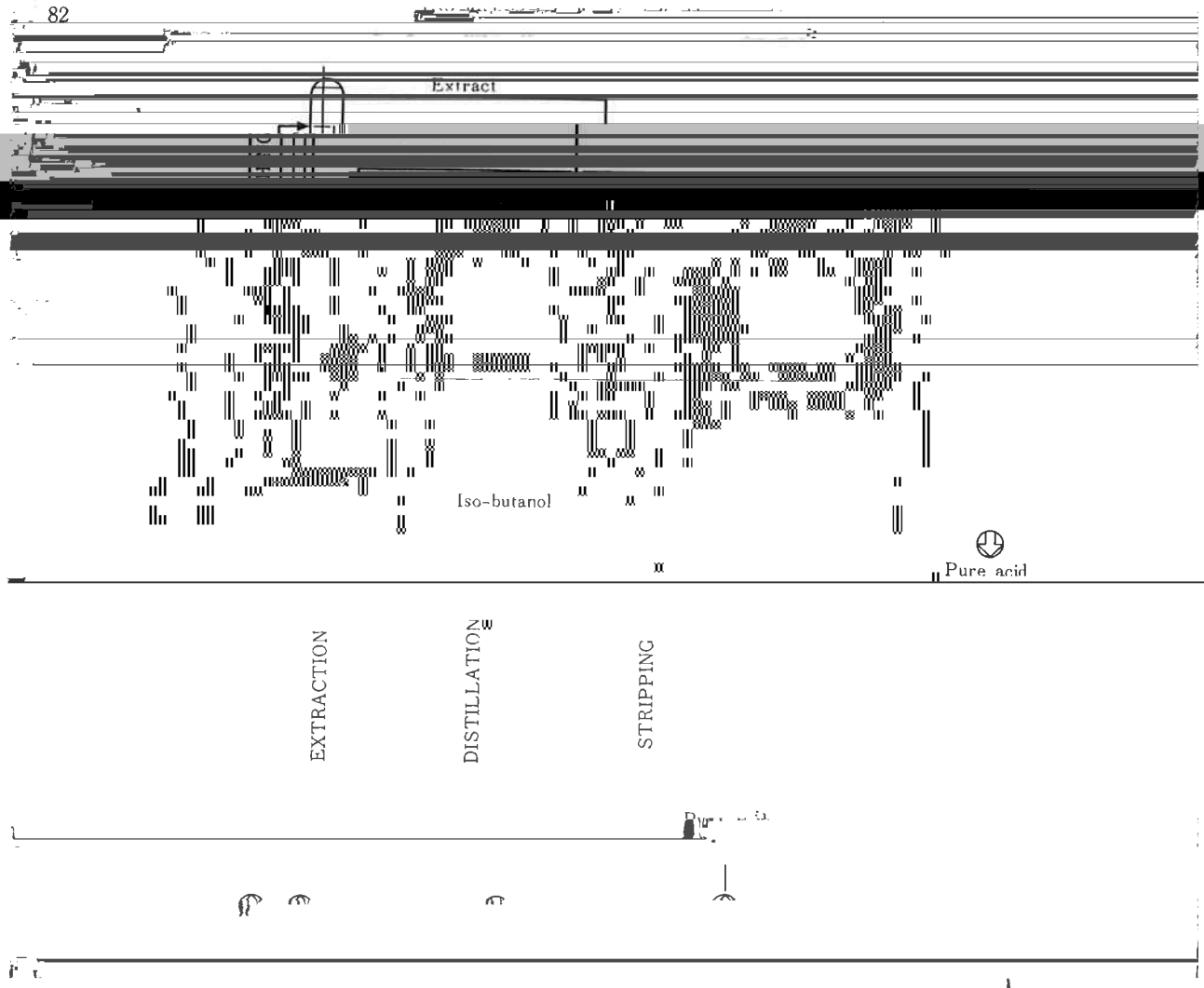


Table 5. Process Parameters (continued)

Crude acid	Extent of	Yield of	Product, acid
100	100	100	100
90	90	90	90
80	80	80	80
70	70	70	70
60	60	60	60
50	50	50	50
40	40	40	40
30	30	30	30
20	20	20	20
10	10	10	10
0	0	0	0

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表 7

リン酸肥料製造の副産物の利用

Table 7 Consumption data of Phocex process

Raw acid	(ton P ₂ O ₅)	1.02	1.02
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Table C-1

S.G.	1.66	1.07	1.
H ₂ O	1.71	0.0	0.1
SO ₂	1.6	0.5	1.
Fe	0.02	0.04	0.0
Mg	0.25	0.02	0.0
MBK	52.0	1.	

1.40
 56
 0.65
 0.0025
 0.0005

1.6

作が必要ないことは一つの特徴である。

である。

Crude	Pure	Pure
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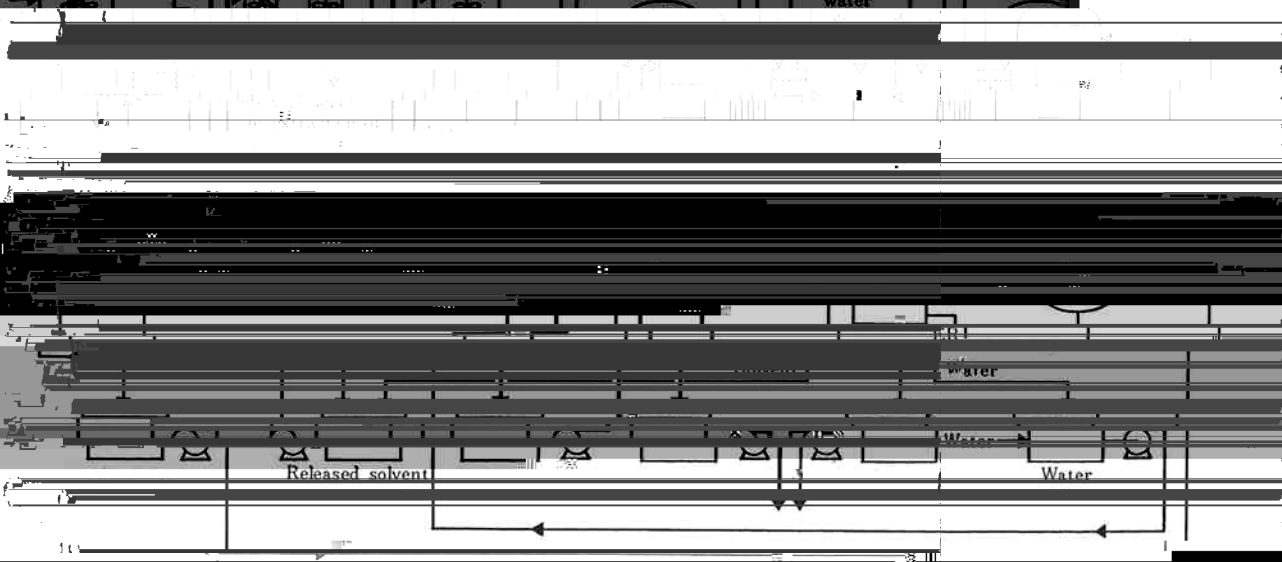
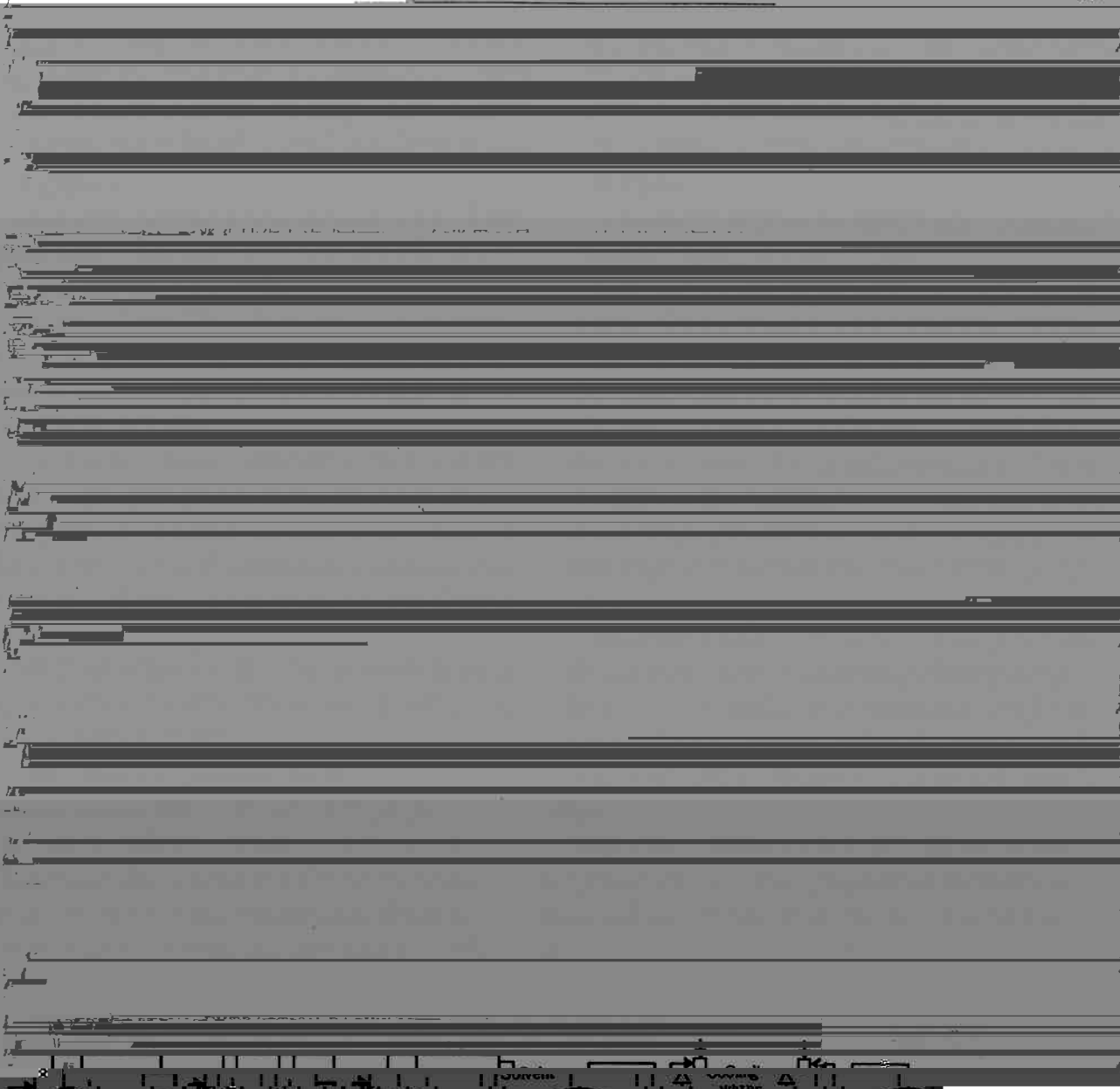


Table 0 D-dl-Citric acid

No.	Solvent	% H ₃ PO ₄	
		60	80
i-Pr ₂ O (5°C)			
		73.5	86.4

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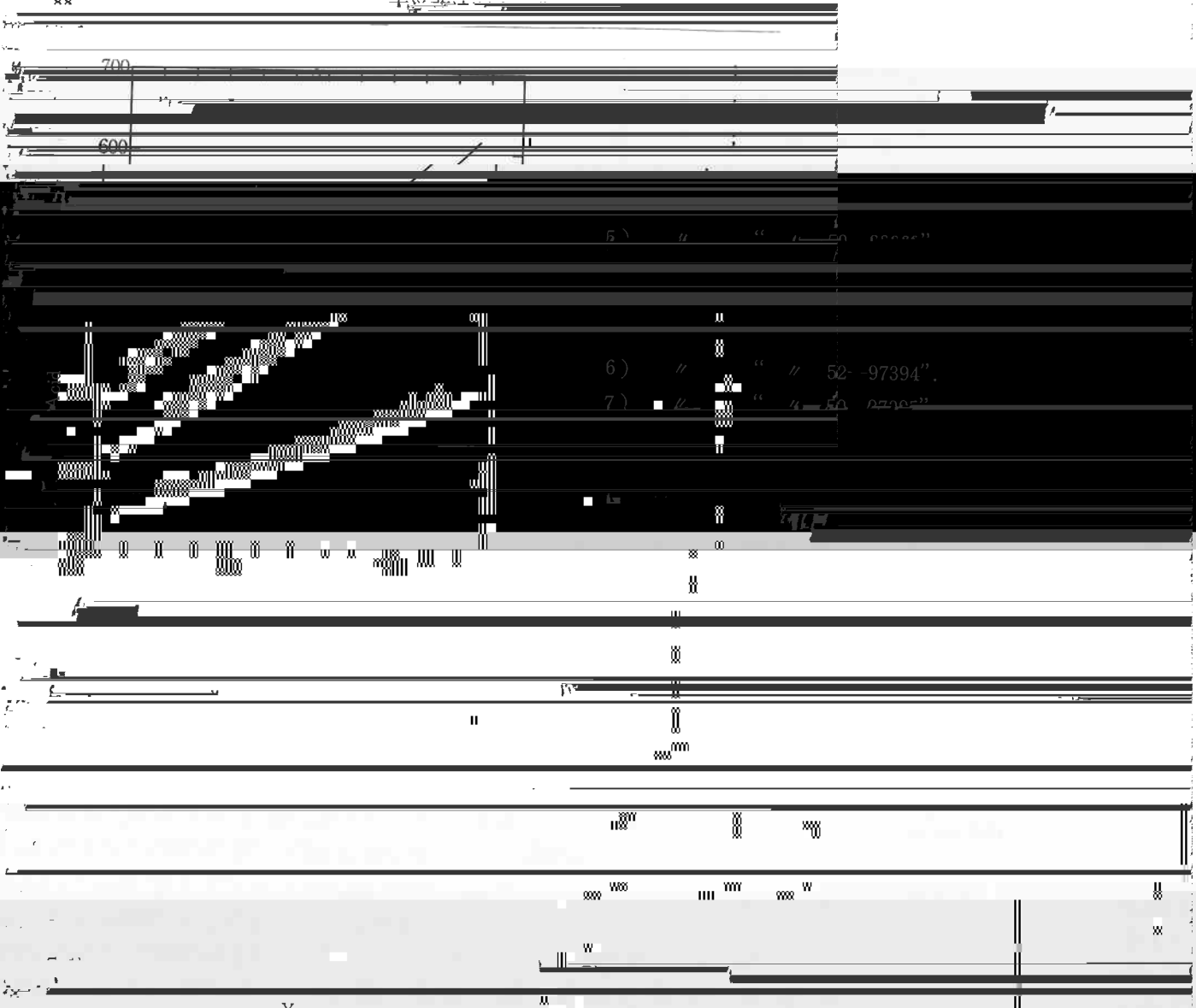


Fig. 9 Assumption of production cost of USSR

